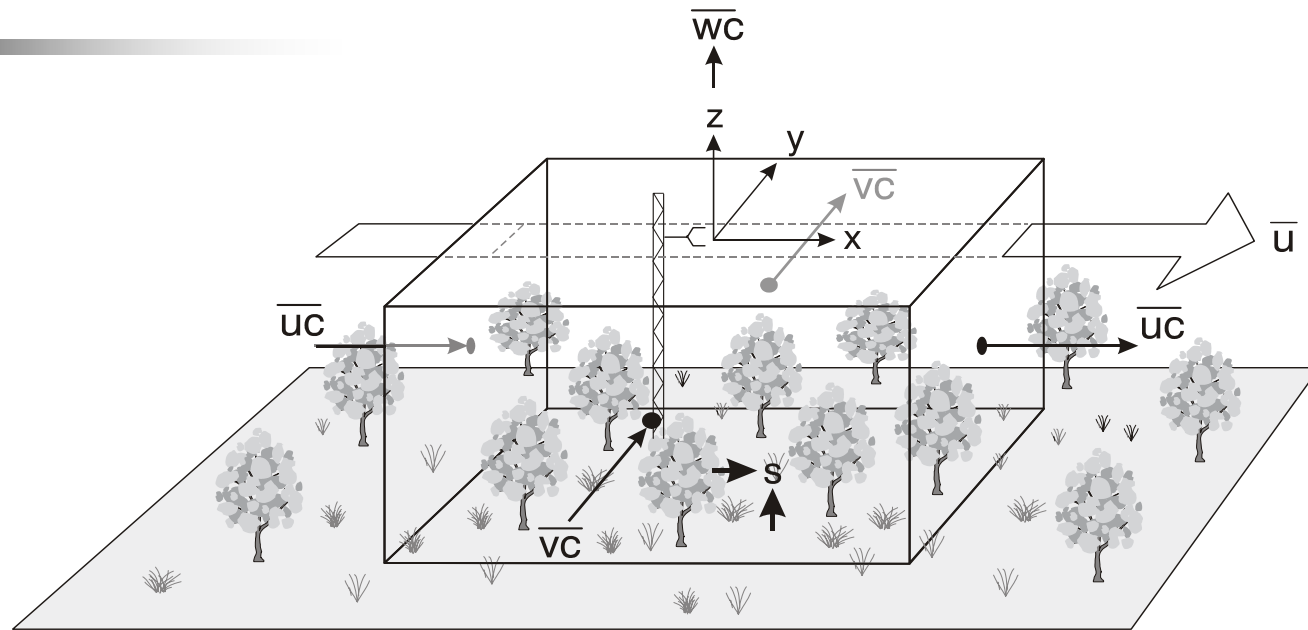




Lecture 3: Eddy flux measurement theory

- Conservation of mass equation for a control volume
- Webb, Pearman & Leuning theory
- Open-path instruments
- Closed-path instruments
- Summary

Control volume over surface around tower



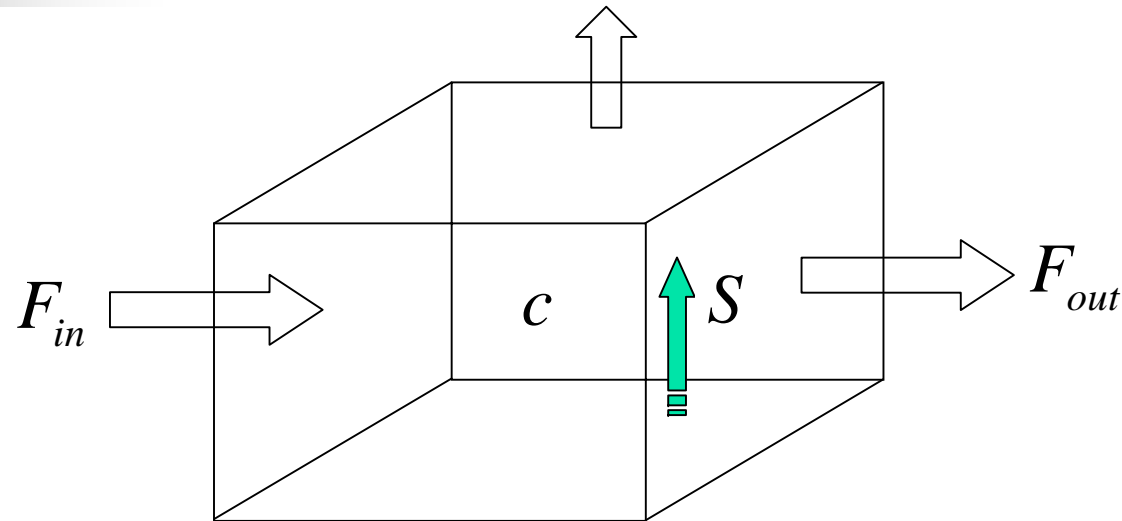
We want sum of CO_2 & H_2O fluxes from soil and plant surfaces within CV

We measure eddy flux at top of tower \overline{wC}

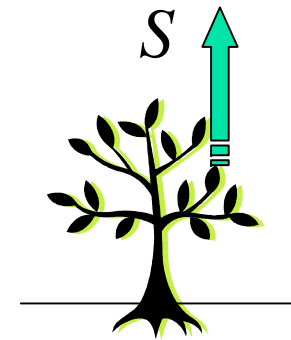
- When are they equal?
- What assumptions, simplifications are needed?

Mass conservation in small volume dV

Leuning (2004, Ch 6)



$$\frac{\partial c}{\partial t} + \nabla \cdot \mathbf{F} = S_d + S_c$$



Use vector notation ($\nabla \cdot \mathbf{F} = \partial F_x / \partial x + \partial F_y / \partial y + \partial F_z / \partial z$)



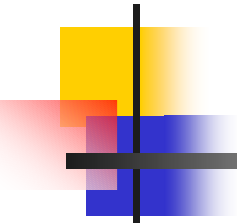
Mass conservation in small volume dV

$$\frac{\partial(c_d + c_c)}{\partial t} + \nabla \cdot (\mathbf{F}_d + \mathbf{F}_c) = S_d + S_c$$

- Consider dry air and quantity c separately

$$\frac{\partial c_d}{\partial t} + \nabla \cdot \mathbf{u} c_d = 0 \quad \text{No sources/sinks of dry air in CV}$$

$$\frac{\partial c_c}{\partial t} + \nabla \cdot \mathbf{u} c_c = S_c \quad \text{Sources/sinks of } c \text{ in CV}$$



Show that $\overline{S_c} = \frac{\partial \overline{c_c}}{\partial t} + \nabla \cdot \overline{\mathbf{u} c_c}$ equals

$$\overline{S_c} = \overline{c_d} \frac{\partial \overline{\chi_c}}{\partial t} + \overline{\mathbf{u} c_d} \cdot \nabla \overline{\chi_c} + \nabla \cdot (\overline{c_d \mathbf{u}' \chi_c'})$$

$\overline{c_d}$ = concentration of dry air

$\overline{\chi_c}$ = mixing ratio of quantity c in dry air

$\mathbf{u} = (u, v, w)$ = velocity vector

$\overline{S_c}$ = source flux density

Reynolds decomposition $\chi_c = \overline{\chi} + \chi_c'$, $u = \overline{u} + u'$

Overbar = time average $\overline{\chi} = (1/\Delta t) \int_t^{t+\Delta t} \chi dt$

Conservation equation for quantity c

$$\overline{\frac{\partial c_c}{\partial t}} + \nabla \cdot \overline{\mathbf{u} c_c} = \overline{S_c}$$

Use **mixing ratio** for c and **Reynolds decomposition**

$$c_c = c_d \chi_c = (\overline{c_d} + c'_d)(\overline{\chi_c} + \chi'_c) \quad \mathbf{u} = (\overline{\mathbf{u}} + \mathbf{u}')$$

↑
↑
↑
 Mixing ratio Mean Fluctuation

$$\overline{\frac{\partial (\overline{c_d} + c'_d)(\overline{\chi_c} + \chi'_c)}{\partial t}} + \nabla \cdot \overline{[(\overline{\mathbf{u}} + \mathbf{u}')(\overline{c_d} + c'_d)(\overline{\chi_c} + \chi'_c)]} = \overline{S_c}$$

After some algebra- see Leuning (2004)

$$\overline{c_d} \frac{\partial \overline{\chi_c}}{\partial t} + \overline{\chi_c} \left[\frac{\partial \overline{c_d}}{\partial t} + \nabla \cdot \overline{\mathbf{u} c_d} \right] + \overline{\mathbf{u} c_d} \cdot \nabla \overline{\chi_c} + \nabla \cdot (\overline{c_d \mathbf{u}' \chi_c'}) = \overline{S_c}$$

$$\overline{c_d} \frac{\partial \overline{\chi_c}}{\partial t} + \overline{\mathbf{u} c_d} \cdot \nabla \overline{\chi_c} + \nabla \cdot (\overline{c_d \mathbf{u}' \chi_c'}) = \overline{S_c}$$

Δ storage

advection

eddy flux
divergence

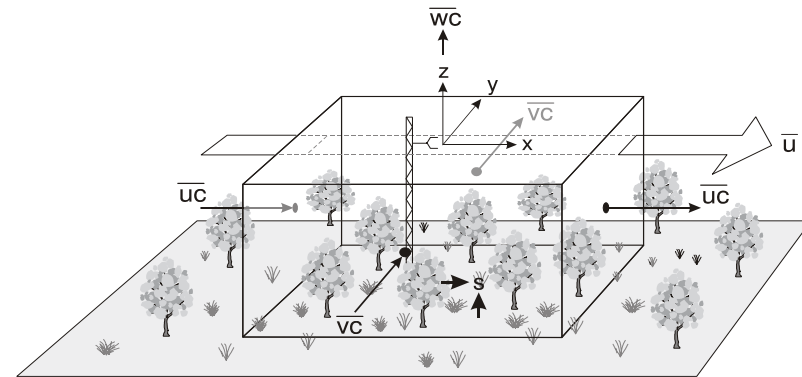
Source flux
density

Mass conservation in CV around flux tower

$$\overline{F_0} = \frac{1}{L^2} \int_0^L \int_0^L \int_0^h \overline{c_d} \frac{\partial \overline{\chi_c}}{\partial t} dx dy dz$$

$$+ \frac{1}{L^2} \int_0^L \int_0^L \int_0^h \left[\overline{uc_d} \frac{\partial \overline{\chi_c}}{\partial x} + \overline{vc_d} \frac{\partial \overline{\chi_c}}{\partial y} + \overline{wc_d} \frac{\partial \overline{\chi_c}}{\partial z} \right] dx dy dz$$

$$+ \frac{1}{L^2} \int_0^L \int_0^L \int_0^h \left[\frac{\partial \overline{c_d u' \chi_c'}}{\partial x} + \frac{\partial \overline{c_d v' \chi_c'}}{\partial y} + \frac{\partial \overline{c_d w' \chi_c'}}{\partial z} \right] dx dy dz$$



Note spatial averaging



Coordinate system

- Have used rectangular Cartesian coordinates
- Can rarely measure all components of mass balance. To maximize information at tower choose site and coordinate system to ensure:

$$\overline{vc_d} = \overline{wc_d} = 0$$

Coordinate rotation (see later)

$$\frac{\partial \overline{\chi_c}}{\partial x}, \frac{\partial \overline{\chi_c}}{\partial y} \rightarrow 0$$

Horizontal homogeneity –
no advection

$$\frac{\partial \overline{w'\chi_c'}}{\partial z} \neq \frac{\partial \overline{u'\chi_c'}}{\partial x}, \frac{\partial \overline{v'\chi_c'}}{\partial y}$$

No horizontal eddy flux
divergence



Horizontally homogeneous flow

$$\begin{aligned}
 \overline{F_0} &= \frac{1}{L^2} \int_0^L \int_0^L \int_0^h \overline{c_d} \frac{\partial \overline{\chi_c}}{\partial t} dx dy dz \\
 &+ \frac{1}{L^2} \int_0^L \int_0^L \int_0^h \left[\overline{u c_d} \frac{\partial \overline{\chi_c}}{\partial x} + \overline{v c_d} \frac{\partial \overline{\chi_c}}{\partial y} + \overline{w c_d} \frac{\partial \overline{\chi_c}}{\partial z} \right] dx dy dz \\
 &+ \frac{1}{L^2} \int_0^L \int_0^L \int_0^h \left[\frac{\partial \overline{c_d u} \chi_c'}{\partial x} + \frac{\partial \overline{c_d v} \chi_c'}{\partial y} + \frac{\partial \overline{c_d w} \chi_c'}{\partial z} \right] dx dy dz
 \end{aligned}$$



Horizontally homogeneous flow

Non-steady-state

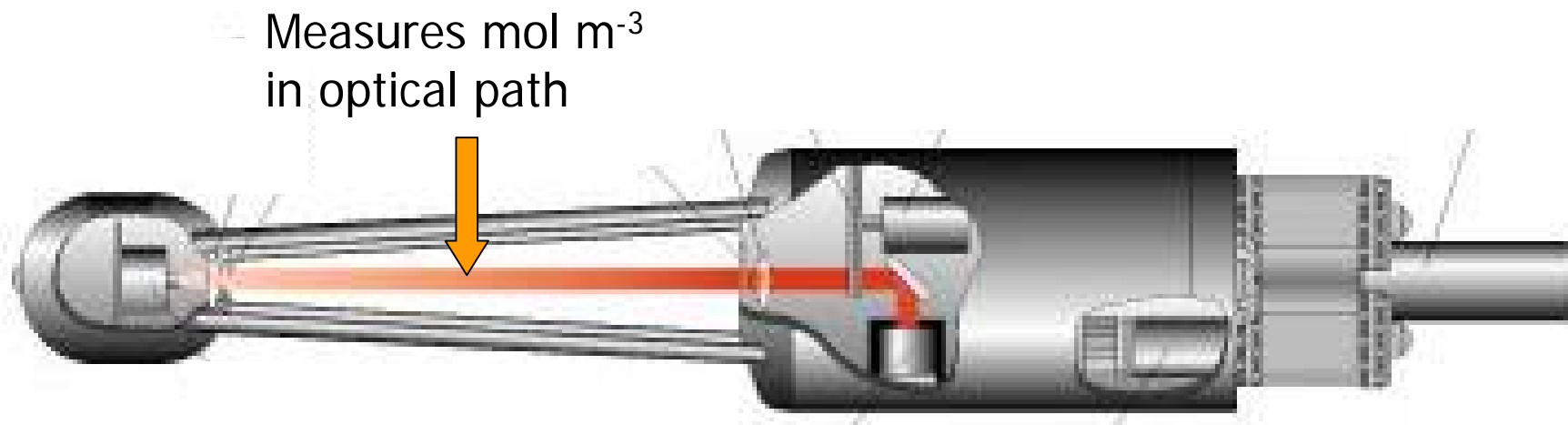
$$\overline{F_0} = \int_0^h \overline{c_d} \frac{\partial \overline{\chi_c}}{\partial t} dz + \overline{c_d} \overline{w' \chi_c'}$$

Steady-state eddy flux

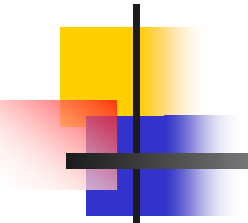
$$\overline{F_0} = \overline{c_d} \overline{w' \chi_c'}$$

Time-averages at a point are assumed equal to space average – ergodic hypothesis

Concentrations measured, not mixing ratios



LI-7500 Open-path CO₂ and water vapor analyser



Webb, Pearman & Leuning (1980) theory (1)
Steady state, horiz. homogeneous flow

$$\overline{F_c} = \overline{wc_c} = \overline{wc_c} + \overline{w'c'_c} \quad \text{Trace gas flux}$$

What is \overline{w} ?

$$\overline{F_d} = 0 = \overline{wc_d} + \overline{w'c'_d} \quad \text{No net flux of dry air}$$

$$\overline{w} = \frac{\overline{-w'c'_d}}{c_d} \quad \text{Need expression for } c'_d$$

WPL theory (2)

$$\overline{w} = \frac{\overline{-w'c'_d}}{c_d}$$

$$c'_d = c' - c'_v$$

$$c = \frac{p}{RT}, \quad c' = -\overline{c} \left[\frac{T'}{\overline{T}} - \frac{p'}{\overline{p}} \right]$$

$$c'_d = -\overline{c} \left[\frac{T'}{\overline{T}} - \frac{p'}{\overline{p}} \right] - c'_v$$

$$\overline{w} = \frac{1}{c_d} \left[\overline{w'c'_v} + \overline{c} \left(\frac{\overline{w'T'}}{\overline{T}} - \frac{\overline{w'p'}}{\overline{p}} \right) \right]$$



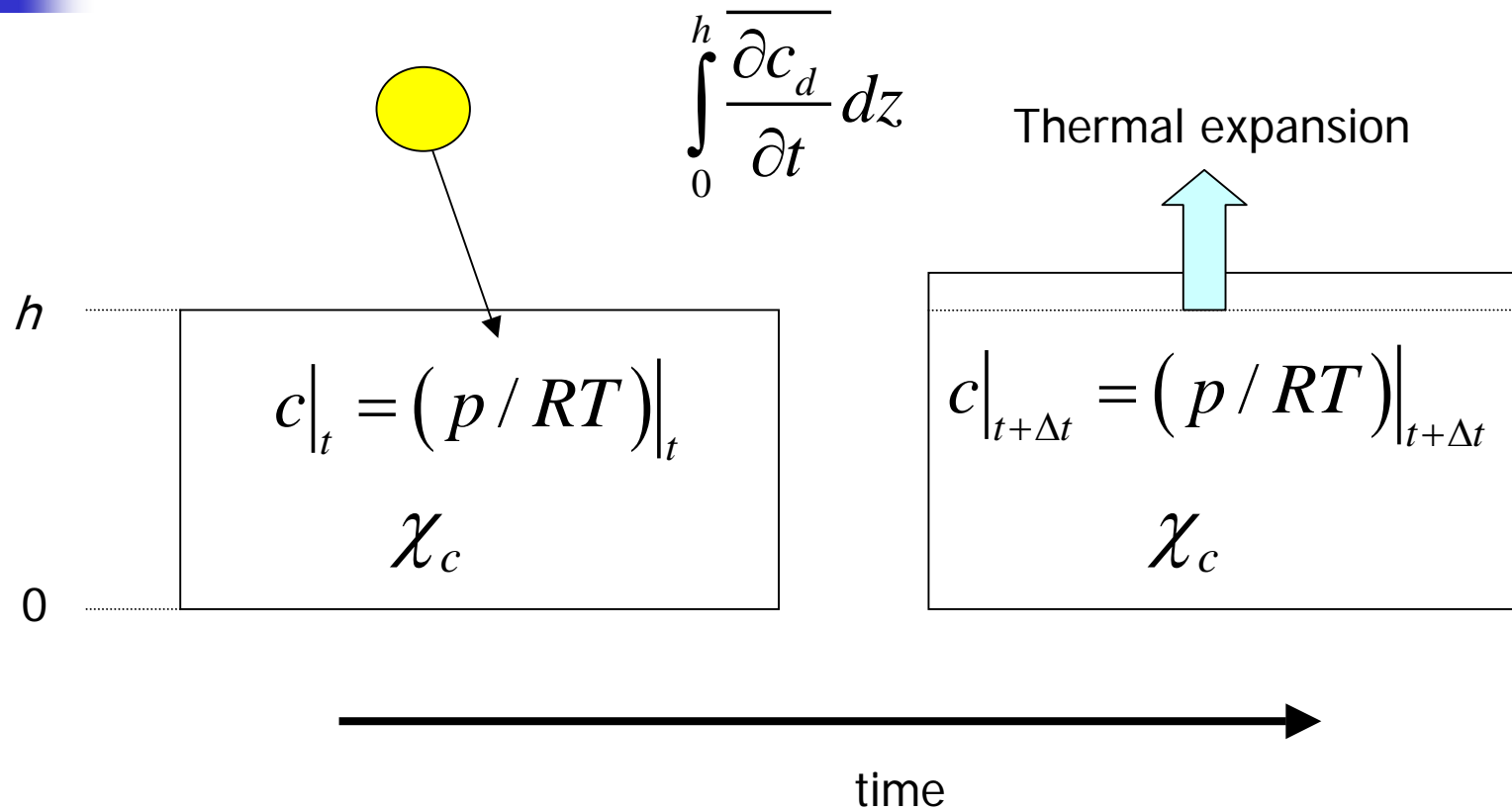
WPL theory (3)

- Open-path instruments

$$\overline{F_0} = \overline{c_d w' \chi_c'} = \overline{w' c_c'} + \chi_c \left[\overline{w' c_v'} + \overline{c \frac{w' T'}{T}} \right]$$

Raw CO₂ flux Water vapor flux Heat flux

Non-steady state, horiz. homogeneous flow



WPL theory (4)

$$0 = \overline{F_d} = \int_0^h \overline{\frac{\partial c_d}{\partial t}} dz + \overline{w c_d} + \overline{w' c_d'} \quad \text{No source/sink of dry air}$$

$$\overline{w} = \frac{-1}{\overline{c_d \Delta t}} \left[\int_0^h (c_d|_{t+\Delta t} - c_d|_t) dz \right] - \frac{\overline{w' c_d'}}{\overline{c_d}}$$

$$\overline{w} = - \frac{\overline{w' c_d'}}{\overline{c_d}}, \quad \text{original WPL}$$

WPL theory (5)

$$\overline{F_c} = \int_0^h \overline{\frac{\partial c_c}{\partial t}} dz + \overline{w c_c} + \overline{w' c_c'}$$

Hand-out notes show that

$$\begin{aligned} \overline{F_c} &= \overline{\frac{\chi_c}{\Delta t} \left[\int_0^h (c_d|_{t+\Delta t} - c_d|_t) dz \right]} \\ &\quad \parallel \\ &= \overline{\frac{\chi_c}{\Delta t} \left[\int_0^h (c_d|_{t+\Delta t} - c_d|_t) dz \right]} - \overline{\chi_c w' c_d'} + \overline{w' c_c'} \end{aligned}$$

$$\overline{F_c} = \overline{w' c_c'} - \overline{\chi_c w' c_d'} = \text{original WPL}$$




How big is \overline{w} ?

- In terms of latent & sensible heat fluxes

$$\overline{w} = 10^{-6} (0.54\lambda\overline{E} + 2.80\overline{H})$$

- $< 3 \text{ mm s}^{-1}$
- Difficult to measure directly

Open path measurements – calculation sequence


$$1) \quad \overline{H} = \overline{\rho c_p} \overline{w' T'}$$

$$2) \quad \overline{E} = (1 + \overline{\chi_v}) \left[\overline{w' c'_v} + \frac{\overline{c_v}}{\overline{T}} \frac{\overline{H}}{\overline{\rho c_p}} \right]$$

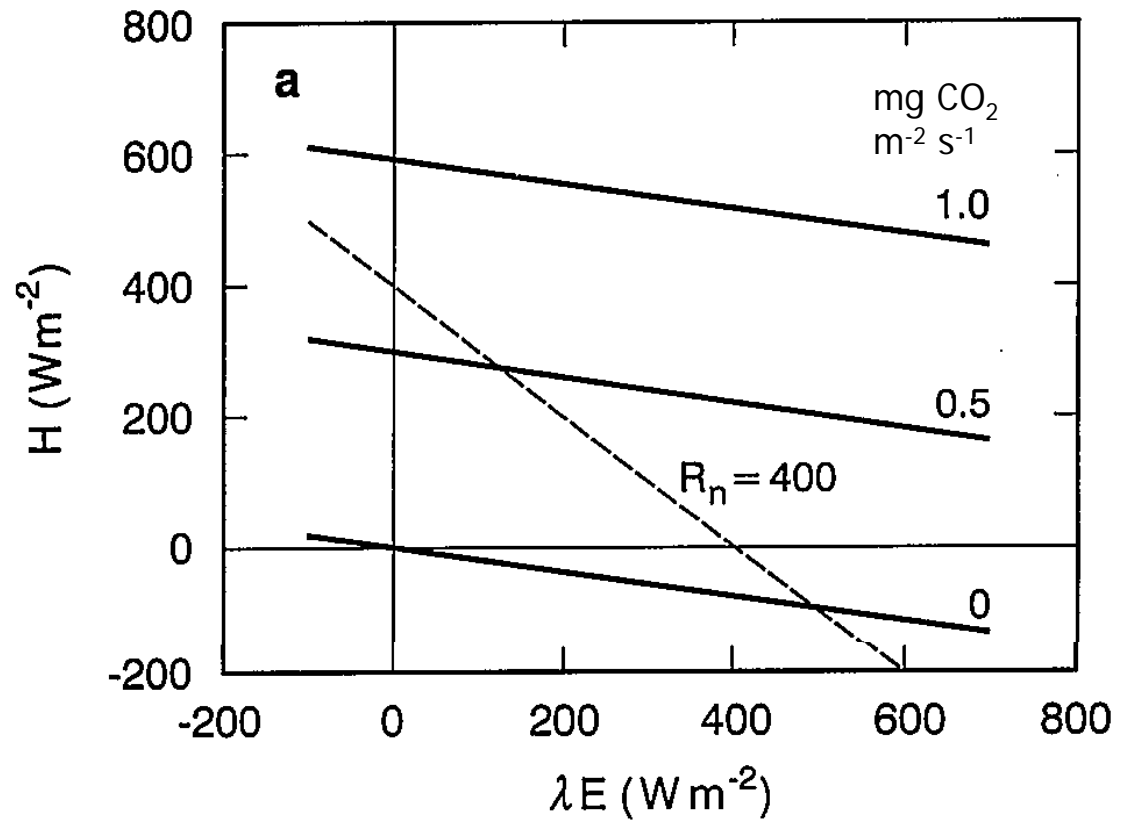
$$3) \quad \overline{F_c} = \overline{w' c'_c} + \overline{c_c} \left[\frac{\overline{E}}{\overline{c}} + \frac{\overline{H}}{\overline{\rho c_p T}} \right]$$

WPL corrections

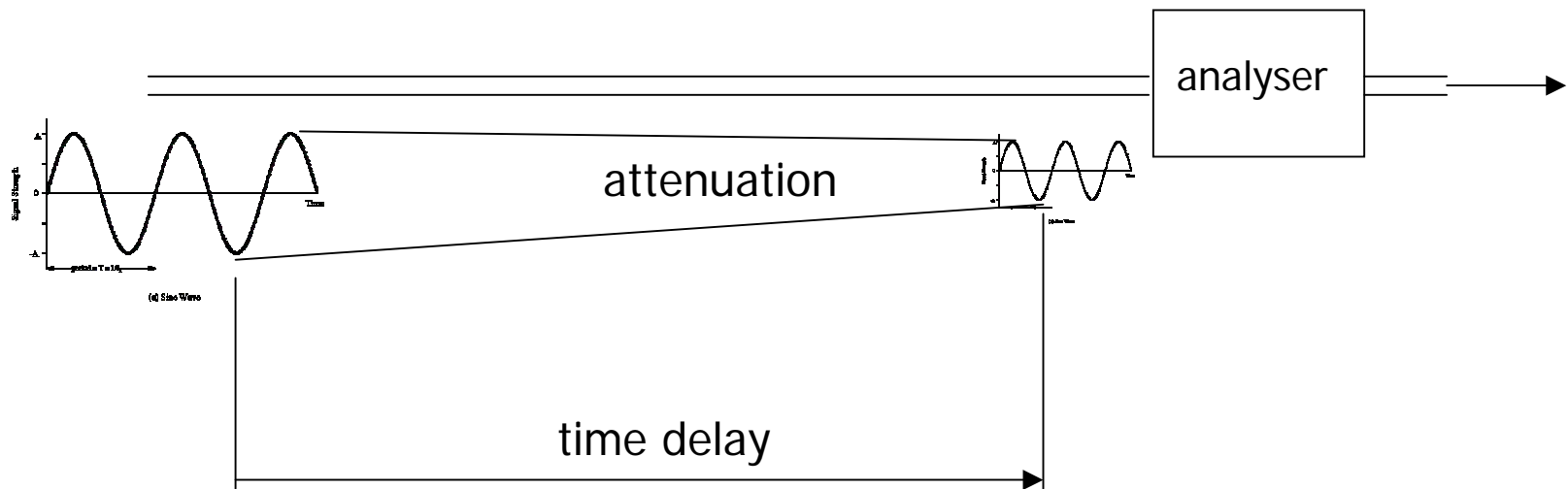
1 mg CO₂ = 22.7 μmol CO₂

$$\overline{F_c} = \overline{w'c'_c} + c_c \left[\frac{\overline{E}}{c} + \frac{\overline{H}}{\rho c_p T} \right]$$

↑
Correction term

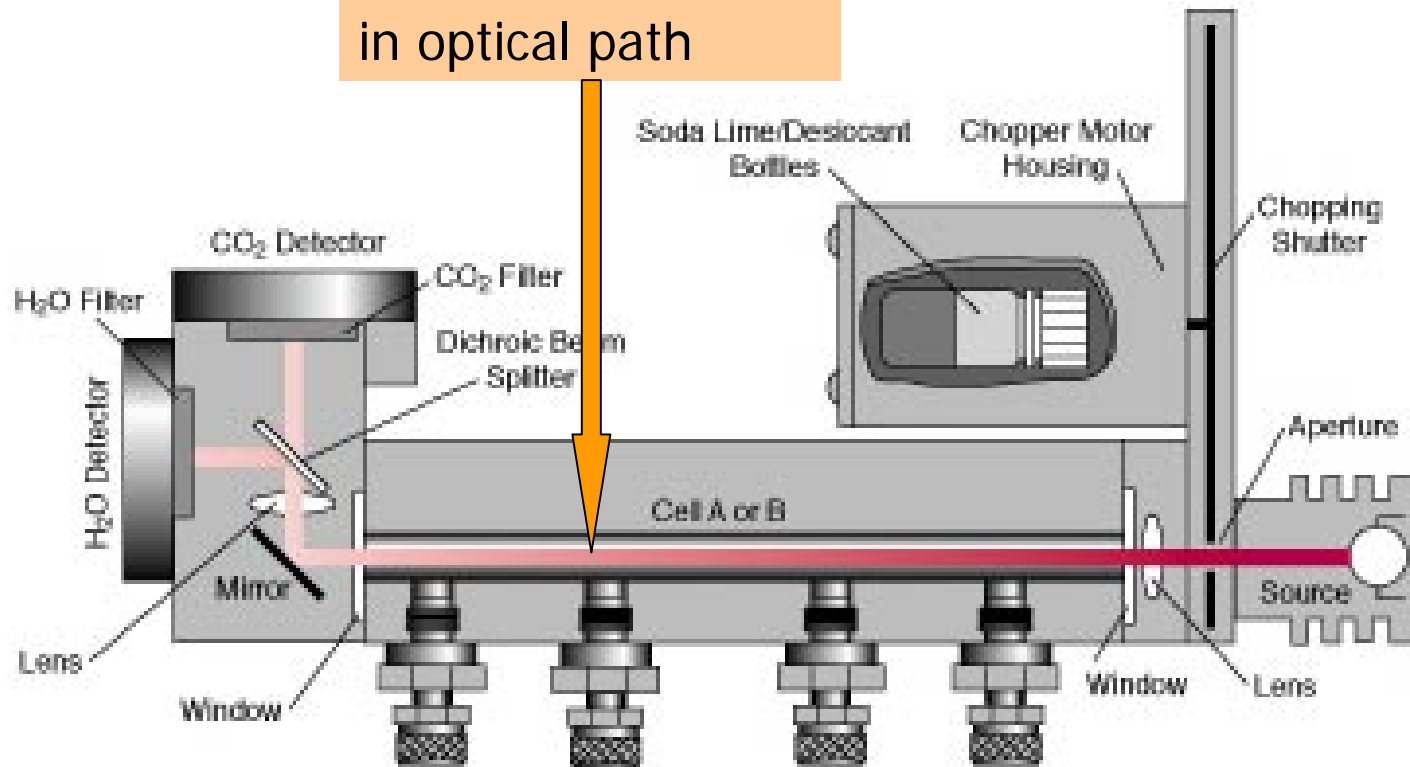


Closed-path gas sampling



Licor 7000 Closed-path analyser

Measures mol m⁻³
in optical path





Closed-path analyser (1)

- T & P fluctuations must be removed for all frequencies $\geq 1/(2\pi t_{av})$
 - Air not dried

$$1) \quad \overline{E} = \frac{\overline{pT}_i}{\overline{p}_i T} (1 + \overline{\chi}_v) \overline{w'c'_v}$$

$$2) \quad \overline{F}_c = \frac{\overline{pT}_i}{\overline{p}_i T} \left[\overline{w'c'_c} + \overline{\chi}_c \overline{w'c'_v} \right]$$



Closed-path analyser (2)

- Measure c_c , c_v , T & P simultaneously in gas analyser and calculate mixing ratio at sampling rate (10 Hz) used for eddy covariance

$$\chi_v = \frac{c_v}{P_i / (RT_i) - c_v}, \quad \chi_c = \frac{c_c}{P_i / (RT_i) - c_c}$$

- Must consider
 - Time-lag
 - Hi-frequency attenuation

Summary



- No net source/sink of dry air in CV
- Flux equation for trace gas is exact using mixing ratios relative to dry air for full, unsteady 3-D flows
- Use existing WPL corrections, even for 3-D flows